



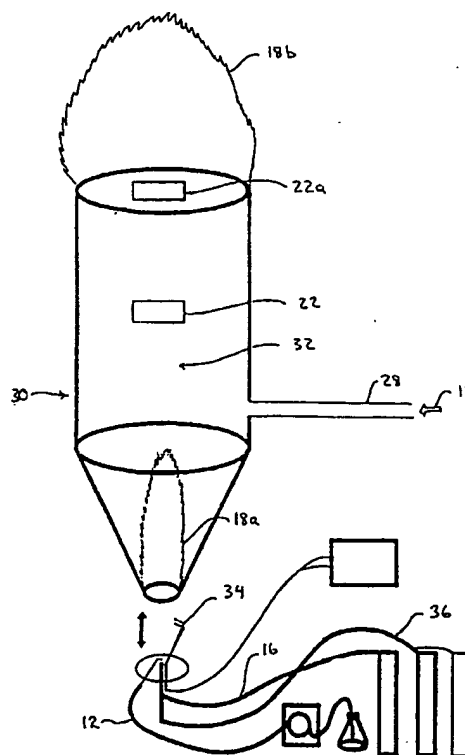
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(54) Title: METHOD AND APPARATUS FOR THE COMBUSTION CHEMICAL VAPOR DEPOSITION OF FILMS AND COATINGS

(57) Abstract

A method for applying coatings to substrates using combustion chemical vapor deposition by mixing together a reagent and a carrier solution to form a reagent mixture, igniting the reagent mixture to create a flame, or flowing the reagent mixture through a plasma torch, in which the reagent is at least partially vaporized into a vapor phase, and contacting the vapor phase of the reagent to a substrate resulting in the deposition, at least in part from the vapor phase, of a coating of the reagent which can be controlled so as to have a preferred orientation on the substrate, and an apparatus to accomplish this method. The figure shows a schematic of a CCVD apparatus where the substrate (22) can be placed within the reducing region (32) of the Smithell separator (30) between the inner flame (18a) and the outer flame (18b).



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**METHOD AND APPARATUS FOR THE COMBUSTION
CHEMICAL VAPOR DEPOSITION OF
FILMS AND COATINGS**

5 **BACKGROUND OF THE INVENTION**

1. **Field of the Invention**

 The field of this invention is related generally to the combustion chemical vapor deposition of reagents by flame onto a substrate under generally ambient conditions, and more specifically to the flame combustion chemical vapor deposition
10 from vapor reagents and/or reagents dissolved in or carried by a flammable liquid organic solution which is burned with an oxidant, vaporizing the reagent, and then depositing the coating from the vapor phase onto a substrate positioned in the resulting hot gas in or just beyond the flame's end.

2. **Prior Art**

15 Over the last century numerous thin film deposition methods have been developed and commercialized. Thin films usually are considered to be less than 10 microns thick. The Handbook of Thin-Film Deposition Processes and Techniques (Noyes Pubs. 1988; Schuegraf, K.K. editor) provides a broad review of thin-film deposition techniques. Of these technologies, chemical vapor deposition, spray
20 deposition and thermal spraying deposition are the most related deposition techniques.

 Chemical Vapor Deposition (CVD) is a materials synthesis process in which constituents of the vapor phase react chemically near or on a substrate surface to form a solid product. In most cases, gas phases flow into a reaction chamber where CVD occurs. The reaction occurs at an elevated temperature which is provided by a furnace
25 or by a method, usually RF induction or high-intensity radiation lamps, to heat the material substrate that is to be coated. Plasma, microwave, photo, laser, RF, and electron-enhanced CVD processes have all been developed. Since a reaction chamber and secondary heat source are mandatory with these processes, they are quite different from the combustion CVD (CCVD) of the present invention, which can be conducted
30 in open-atmosphere without the need for a secondary heat source.

 In the 1940's, a CVD process utilizing a flame to produce homogeneously nucleated (powder) oxides of titanium, zirconium, iron, aluminum, and silicon was developed as disclosed in Swiss Patent No. 265192. By injecting a metal halide vapor and oxygen mixture through the central nozzle of a burner, fuel gas through an
35 intermediate ring, and oxygen through the outer ring, a flame was produced from the

burner. The 950°C to 1000°C temperature of the flame caused oxidation of the metal halide vapor, which condensed to form very fine oxide powders.

United States Patents Nos. 2,239,551, 2,272,342, and 2,326,059 were granted for producing glass and glass coatings in a flame using combustible gases and the
5 vapor of a hydrolyzable compound of silicon solely or with other possible volatile compounds providing one or more additional oxides such as titania or alumina. These methods use only gas and/or vapor source materials to produce glass coatings, whereas the present method uses a liquid solution to produce glass coatings.

Diamond (carbon) films have been deposited utilizing the inner flame region
10 (reducing region) of a combustion flame of acetylene and oxygen with the carbon source provided by the decomposition of acetylene. Hirose, Y., et al., The Synthesis of High Quality Diamond in Combustion Flame, 89 - 12 Proc. Electrochem. Soc. (1989); Zhu, W. et al., Growth and Characterization of Diamond Films on Non-Diamond Substrates for Electronic Applications, IEEE Proceedings, May 1991, pp.
15 621 - 46; Murakawa, M. et al., An Experiment in Large Area Diamond Coating Using a Combustion Flame Torch in its Traversing Mode, Surf. and Coatings Tech., pp. 22 - 9 (Dec. 5, 1990). Two-component oxide powders have been made via a combustion flame in a reactor using all vapor sources mixed with nitrogen in a hydrogen-oxygen flame. Hori, S. et al., Characterization and Processing of CVD Powders for
20 Fabrication of Composite and Compound Ceramics, 155 Mat. Res. Soc. Symp. Proc. pp. 3 - 12 (1989). Carbon black coatings form on materials held in or beyond oxygen deficient flames. For diamond and other pure carbon films, the carbon is deposited from the fuel itself; however, with the present method, a reagent from which the coating is formed is introduced in addition to the fuel.

CVD has been accomplished using a sprayed or atomized solution. Groth, R.,
25 14 Phys. Stat. Sol., p. 69 (1966). One such process, the Pyrosol® process, involves the deposition from a vapor produced from an aerosol generated by ultrasonically nebulizing a solution of organic or inorganic compounds into a furnace. Blandenet, G. et al., Indium Oxide Deposition on Glass by Aerosol Pyrolysis, 5th Int'l. Conf. on
30 CVD, p. 190 - 203 (1975). Another method, Pyrolytic Spray™, produces aluminum coatings by atomizing warmed aluminum alkyl, as either a pure liquid or as a kerosene dilution, over a heated substrate in a reaction chamber. Withers, J.C. et al., Aluminum Coatings by a Pyrolytic Spray CVD Process, Second. Int'l Conf. on CVD, p. 393 - 402 (1970). These reactions are confined to a reaction chamber or furnace
35 and call for an external heat source. The basic concept is that the atomized liquid vaporizes prior to reaching the substrate, and then reacts on or near the substrate as in

conventional CVD. None utilize a flame or combustion, as does the present invention.

CVD has been accomplished by directly feeding reactive powders such as metal-organics or halides into a furnace. Hollabough, C.M. et al., Chemical Vapor
5 Deposition of ZrC Made by Reactions of $ZrCl_4$ with CH_4 and with C_3H_6 , 35 Nucl. Tech., p. 527 - 35 (1977); U.S. Patent No. 4,202,931; Lackey, W.J. et al., Rapid Chemical Vapor Deposition of Superconducting $YBa_2Cu_3O_x$, 56-12 Appl. Phys. Lett., pp. 1175-7 (1990); U.S. Patent No. 5,108,983. When viewing this metal-organic powder feeding CVD technique through a specially designed end cap on the
10 furnace, the powders flashed or combusted in the hot zone of the furnace. The quality of films (vapor deposited) produced by this process suggests that the powder metal components are vaporized during burning. This is very different from using a liquid solution, and requires use of a furnace, unlike CCVD.

United States Patent No. 3,883,336 discloses a method of producing glass in a
15 flame which appears to be a CVD process even though CVD is not mentioned. A flame from a combustible gas and oxygen mixture is combined with additional oxygen containing silicon tetrachloride vapor which intersects the aerosol of an aqueous salt mixture producing a transparent, homogeneous glass body consisting of at least two constituent oxides. In one of the examples listed, a methanol solution is
20 nebulized and burned by the intersecting flame. The claims only cite the use of aqueous solutions. This procedure is more complicated than CCVD, requiring two nozzles. Further, this procedure is used to make glass bodies and forms, not coatings and films as in CCVD.

Spray pyrolysis is a thin film forming technique in which a solution is sprayed
25 onto a heated substrate, thus forming a film. The film commonly receives additional heat treatment to form the desired phase. One spray deposition method uses metal/2-ethyl hexanoates, spin coated onto a substrate which later is heated to pyrolyze the film and form a $YBa_2Cu_3O_x$ (123) film. Gross, M.E. et al., Versatile New Metalorganic Process for Preparing Superconducting Thin Films, Appl. Phys. Lett.,
30 pp. 160 - 2 (Jan. 11, 1988). Another method deposits 123 films by spraying nitrate solutions onto substrates at $180^\circ C$ followed by heat treating and annealing. Gupta, A. et al., $YBa_2Cu_3O_x$ Thin Films Grown by a Simple Spray Deposition Technique, Appl. Phys. Lett., pp. 163 - 5 (Jan. 11, 1988). A third method, U. S. Patent No. 5,002,928, forms oxide superconducting films by ultrasonic wave spraying a
35 homogeneous solution or solutions, organic or inorganic, containing as solutes the metal compounds capable of forming the superconductor onto a heated substrate to

form the thin film. The substrate temperature can be high enough so that later firing is not needed. These processes do not have a flame and do require heating of the substrate during and/or after deposition, unlike the CCVD of the present invention.

Most thermal spraying methods produce thick films (>10 microns) by feeding
5 powder into a gas combustion torch (flame spraying) apparatus or a plasma torch (plasma spraying) device to melt the powdered coating material, which then is splattered onto the object being coated, thus forming a film. Matejka, D. et al., Plasma Spraying of Metallic and Ceramic Materials (John Wiley & Sons, 1989). Thermal spraying in general is considerably different from CVD and CCVD. An
10 extension of thermal spraying is physical vapor deposition by vaporizing the powdered material, in which the boiling point of the material is exceeded in the thermal sprayer. The resulting vaporized materials then condense on the cooler substrate. This evaporation technique was used early in high temperature superconductor research, and formed c-axis preferred orientation of 123 at deposition
15 rates of up to 10 microns/min. Terashima, K., Preparation of Superconducting Y-Ba-Cu-O Films by a Reactive Plasma Evaporation Method, Appl. Phys. Lett., pp. 1274 - 6 (April 11, 1988). When only a melting of the 123 was performed, no preferred orientation to the deposited 123 was observed, and the resulting electrical properties were similar to bulk materials. Pawlowski, L. et al., Properties of Plasma Sprayed
20 123 High Temperature Superconductors, Proc. Third National Thermal Spray Conf., p. 641 - 6 (May 1990). Most thermal spray processes try to minimize the amount of evaporated powder, because this reduces the efficiency, that is, the ratio of deposited material to in-fed material, of the deposition process. Varacalle, D.J. et al., Plasma Spraying of Zirconia Coatings, 155 Mat. Res. Soc. Symp. Proc., pp. 235 - 46 (1989).
25 The films resulting from this process can be very similar to CVD films, but the process is different.

A variation of flame spraying is the feeding of a solution instead of a powder into a flame. Atomized nitrate solutions of Y, Ba and Cu have been reacted in an oxyhydrogen flame to produce fine superconducting powders. Zachariah, M.R. et al.,
30 Aerosol Processing of YBaCuO Superconductors in a Flame Reactor, 6 J. Mater. Res., No. 2, pp. 264 - 9 (Feb. 1991); Merkle, B.D. et al., Superconducting $\text{YBa}_2\text{Cu}_3\text{O}_x$ Particulate Produced by Total Consumption Burner Processing, A124 Mat. Sci. Eng., pp. 31 - 8 (1990). The flame vaporizes the water, leaving the Y, Ba and Cu nitrate particles which react with the flame's OH and O radicals, causing oxidation to yield a
35 123 particle. A stoichiometric $\text{H}_2\text{-O}_2$ flame temperature is about 2600°C at atmospheric pressure, but the flame is cooled, by the solution and the addition of Ar,

to the 700-1100°C range so that vaporization of Y, Cu and Ba is minimized. In this variation, the heat source is not the solution, and the end material is a powder. The best powders were made using a diffusion flame with a flame temperature of 700-900°C, likely resulting from an over-ventilated diffusion flame, because of the
5 reduced flame temperature in which 123 is a stable phase and the decreased concentration of water vapor minimizing the formation of BaCO₃. The resulting 123 particles deposited on a platinum substrate just beyond the flame typically are in the 20 to 300 nanometer range. The flame also heated the substrate to a temperature of 550-650°C. The resulting 200 micron thick film from a one hour deposition was
10 particulate in nature with no preferred orientation.

As can be seen, the prior art chemical vapor deposition processes require very specific operating conditions, apparatuses and reactants and carriers. Even with such parameters, many of the prior art processes result in thick films or films with no preferred orientation. Thus, it can be seen that a simple chemical vapor deposition
15 method and apparatus is highly desired but not available. It is to this goal that the present method and apparatus is directed; that is, a flame combustion chemical vapor deposition process in which the reagents are mixed with an oxidant, passed through a torch and burned to form a hot gas containing the vaporized reagents, which is then contacted with a substrate, resulting in the desired coating being deposited on the
20 substrate.

BRIEF SUMMARY OF THE INVENTION

The present invention is a new processing method of and apparatus for chemical vapor deposition (CVD), termed combustion CVD (CCVD). The key to the
25 invention is the direct combustion of flammable liquids or vapors which contain the elements, or reagents, to be deposited on a substrate material. Organic solvents are sprayed or atomized in an oxidizing gas and burned. In the preferred embodiment, the materials to be deposited are in solution; therefore, the mixture is uniform, making the deposition of multicomponent films easier.

30 The substrate material to be coated does not need to be heated in a furnace or reaction chamber. The heat of combustion provides the needed conditions for the reaction of the reagents. The substrate material being coated is likewise heated by the combustion flame, creating the proper kinetic environment for surface reactions, diffusion, film (coating) nucleation and film (coating) growth. The substrate material
35 being coated needs to be located in a zone proximate to the flame's end so that the solutes are dispersed in the hot combustion gases, but not so far from the flame's end

that homogeneous nucleation in the gas stream occurs. By diluting the solution, homogeneous nucleation can be inhibited.

The solutes used need to be properly reactive to form the desired coating. While oxides are the preferred material, other elemental coatings and compounds, for example nitrides, carbides, and carbonates, also can be deposited: An example of an elemental metal coating is silver if the substrate temperature is maintained above the AgO stability temperature. It also is possible to supply only enough oxygen to partially burn the solution so as to form a hot gas which is reducing, and then deposit a material which needs a reducing environment to form.

The method is a simple and inexpensive method for producing many of the same or similar materials which currently are produced by other chemical vapor deposition methods. With a furnace not being necessary, and being conducted in an open-atmosphere environment, much greater flexibility is provided. Large and unusual shapes can be coated completely or only in certain areas as the flame is directed. The invention will become more apparent to one skilled in the art when the following detailed description of the preferred embodiments is read in conjunction with the appended figures.

BRIEF DESCRIPTION OF THE FIGURES

Fig. 1 is a schematic of the combustion chemical vapor deposition apparatus of the present invention.

Fig. 2 is an X-ray diffraction pattern of $\text{YBa}_2\text{Cu}_3\text{O}_x$ CCVD coating on a single crystal MgO substrate prior to post-deposition heat treatment.

Fig. 3 is a resistance versus temperature graph of $\text{YBa}_2\text{Cu}_3\text{O}_x$ CCVD coating on a single crystal MgO substrate after post-deposition heat treatment.

Fig. 4 is a cross-section of a photomicrograph of a YSZ CCVD coating on sapphire.

Fig. 5 is a reflected light photomicrograph of a Y_2BaCuO_5 CCVD coating on an MgO substrate.

Fig. 6 is an X-ray diffraction pattern of a YSZ CCVD coating on an MgO substrate using AcAc precursors.

Fig. 7 is an X-ray diffraction pattern of a YSZ CCVD coating on an MgO substrate using ZEH reagents.

Fig. 8 is an X-ray diffraction pattern of a BaTiO_3 CCVD coating on the side of an MgO substrate opposite the flame using 2EH reagents.

Fig. 9 is an X-ray diffraction pattern of an Ag CCVD coating on an MgO substrate using Ag nitrate as a reagent.

Fig. 10 is a photomicrograph of a cross-section of a BaTiO₃ CCVD coating on an MgO substrate.

5

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

Combustion CVD (CCVD) is the vapor deposition of a film onto a substrate near or in a flame which causes the reagents fed into the flame to chemically react. The present invention discloses CCVD of crystalline, inorganic films beyond the
10 simple carbon black or diamond films, and glass coatings (utilizing a sprayed solution) of the prior art. Flammable organic solvents containing elemental constituents of the desired coating in solution as dissolved reagents are sprayed through a nozzle and burned. Alternatively, vapor reagents can be fed into the flame and burned. Likewise, non-flammable solvents can be used with a gas-fueled flame.
15 An oxidant, such as oxygen, is provided at the nozzle to react with the solvent during burning. Upon burning, reagent species present in the flame chemically react and vaporize, and then deposit and form a coating on a substrate held in the combustion gases in or just beyond the flame's end. During the deposition of oxide coatings, oxygen is available from at least three possible sources: the oxidant gas; the
20 surrounding gases; and the dissolved chemical reagents.

In CCVD, the environment required for CVD to occur is provided by the flame. No furnace, auxiliary heating, or reaction chamber is necessary. Further, CCVD can be carried out in open-atmosphere conditions. The flame supplies the energy needed for CVD in the forms of the kinetic energy of the species present and
25 radiation. This energy creates the appropriate thermal environment to form reactive species and coincidentally heats the substrate, thus providing the conditions for surface reactions, diffusion, nucleation, and growth to occur. When using combustible solutions, the solvent plays two primary roles in CCVD. First, the solvent conveys the coating reagents into the vicinity of the substrate where CVD
30 occurs, thereby allowing the use of low cost soluble precursors. Uniform feed rates of any reagent stoichiometry can be produced easily by simply varying the reagents concentrations in solution and the solution flow rate. Second, combustion of the solvent produces the flame required for CCVD.

In general, CCVD is performed under ambient conditions in the open
35 atmosphere to produce a film on a substrate. The film preferably is crystalline, but may be amorphous, depending on the reagent and deposition conditions used. The

reagent, or chemically reactive compound, is dissolved or carried in a solvent, typically a liquid organic solvent, such as an alkene, alkide or alcohol. The resulting solution is sprayed from a nozzle using oxygen-enriched air as the propellant gas and ignited. A substrate is maintained at or near the flame's end. Flame blow-off may be prevented by use of a hot element such as a small pilot light. The reactants vaporize in the flame and are deposited on the substrate as a film. Resulting films (coatings) have shown extensive preferred orientation in X-ray diffraction patterns, evidencing that CVD occurred by heterogeneous nucleation and resulting in a film having a preferred orientation.

Alternatively, depositions can be performed by feeding solution through a nebulizer, such as a needle bisecting a thin high velocity air stream forming a spray which is ignited and burned. In this manner, other materials, such as Y_2O_3 stabilized ZrO_2 (YSZ), are deposited onto substrates, such as single crystal MgO and sapphire substrates. Two different solvents, ethanol and toluene, and two different metal-organic precursors, acetylacetonates (AcAc) and 2EH, are preferred and were used in the depositions of YSZ given as examples herein. Other reactants and solvents are appropriate and will function in the present invention, as long as a flame can be created which will vaporize the reactants. For example, coatings of $BaTiO_3$, Y_2BaCuO_5 , YIG ($Y_3Fe_5O_{12}$), and Ag also have been deposited.

By considering flame concepts, certain deposition conditions are preferred. First, the substrate needs to be located in a zone such that it is heated by the flame's radiant energy and the hot gases produced by the flame sufficiently to allow surface diffusion. This temperature zone is present from about the middle of the flame to some distance beyond the flame's end. The temperature of the flame can be controlled to some extent by varying the oxidant-to-fuel ratio as well as by adding non-reactive gases to the feed gas or non-combustible miscible liquids to the solution. Secondly, the metal complexes need to be vaporized and chemically changed into the desired state. For oxides, this will occur in the flame if sufficient oxygen is present. The high temperatures, radiant energy (infrared, ultraviolet and other radiant energy), and plasma of the flame aid in the reactivity of precursors. Finally, for single crystal films, the material being deposited should be in the vapor phase, and not stable particles. Particle formation can be suppressed by maintaining a low concentration of solutes, and by minimizing the distance, and therefore time, between where the reagents react and where the substrate is located. Combining these different factors predicts the best CVD deposition zone to be in the proximity of the flame's end. If a solution is sprayed, droplets can strike a substrate located too far into the flame,

possibly resulting in some spray pyrolysis characteristics in the resulting film. A mixture of CVD and spray pyrolysis may be desired in some films. In fact, in some configurations, with large droplets or with some reactants, it may be impossible to not have some spray pyrolysis occur.

5 In general, as long as a flame is produced, CCVD can occur, independent of the flame temperature, deposition zone pressure or temperature, or substrate surface temperature. The flame temperature is dependent on the type and quantity of reagent, solvent, fuel and oxidant used, and the substrate shape and material, and can be determined by one skilled in the art when presented with the particular reagent,
10 solvent, fuel, oxidant and other components and conditions for deposition. The preferred flame temperature for the preferred solutions and materials is between about 300°C and

2800°C. As flames can exist over a wide pressure range, CCVD can be accomplished at a pressure from about 10 torr to about 10,000 torr. Likewise, if a plasma is formed
15 for depositing the coating, the temperature of the plasma can range from about 800°C to about 10,000°C. The temperature of the substrate during the CCVD process also can vary depending on the type of coating desired, the substrate material, and the flame characteristics. Generally, a substrate surface temperature of between about 100°C and 2200°C is preferred.

20 If the droplets actually contacted the substrate, a mixed deposition technique of both CVD and spray pyrolysis may occur. As a droplet approaches the substrate, the outer surface of the droplet may be enriched in the solutes as the solvent was evaporated. The impacting drop should burn off of the substrate almost
instantaneously, possibly cooling and then heating this area, leaving a ring-shaped
25 spot. The ring could be thicker on the outside as more of the solutes would have been concentrated there. This type of deposition might help increase the deposition efficiency, while maintaining heterogeneous nucleation.

Flame chemistry has not been considered in detail as flames are a very complex phenomena and not fully understood chemical reaction environment.
30 However, flame characteristics can be controlled by: varying the gas to fuel ratio beyond stoichiometric to control the flame temperature; altering the type of fuel to effect temperature, luminescence and smoking; mixing the solvents with non-flammable liquids to change the flame characteristics; decreasing the oxygen content to initialize and then increase carbon deposition; depositing non-oxide phases in the
35 reducing environment maintained between the inner and outer flame cones produced with a Smithell separator as shown in Fig. 1c, by feeding reactive gases into the

Smithell separator; reducing droplet size to cause a liquid fuel flame to behave like a premixed gas flame, because the solvents are able to vaporize prior to entering the flame; adjusting nozzle configuration and flow rates to control flame shape and velocity; and reducing the pressure because, depending on fuel and oxidizer, many
5 flames are stable down to pressures of 10 torr.

The deposition rate of the coating onto the substrate can vary widely depending on, among other factors, the coating quality, the coating thickness, the reagent, the substrate material and the flame characteristics. For example, longer coating times can result in thicker coatings, assuming a relatively constant feed flow
10 rate to the flame, less porous coatings, assuming a relatively lower feed flow rate to the flame, or more porous coatings, assuming a relatively greater feed flow rate to the flame. Likewise, if a higher quality coating is desired, a longer coating time at a lower feed flow rate may be necessary, while a gross coating can be produced relatively quickly using a greater feed flow rate. One skilled in the art can determine
15 the feed flow rates and deposition times necessary to produce a desired coating. The preferred deposition rates are from 0.1 $\mu\text{m/hr}$ to 1000 $\mu\text{m/hr}$.

Referring now to Fig. 1a, generalized schematic of the apparatus 10 used to carry out the combustion chemical vapor deposition of the present invention which
20 produces a turbulent flame with no separate inner and outer flames to speak of is shown. A solvent-reagent mixture, which can be flammable or non-flammable solvents mixed with liquid, vaporous or gaseous reagents, but typically is a solvent-reagent solution 12, is supplied to a torch 14 or other flame-producing apparatus. The solvent-reagent solution 12 is ignited in the presence of an oxidant 16, resulting in a
25 flame 18. The solvent-reagent solution 12 may be ignited using any conventional method, and the flame 18 may be maintained, if necessary, by a device such as a conventional pilot light (not shown) or sparker 34 shown in Fig. 1c. As the solvent-reagent solution 12 burns, the reagent vaporizes and leaves the flame 18 along with other hot gases 20 and combustion products. The apparatus 10 shown in Fig. 1b is
30 similar to the apparatus 10 shown in Fig. 1a, but is configured for a non-turbulent flame, suitable for gas reagents and non-flammable carrier solutions. Flame 18 produced by torch 14 of Fig. 1b typically has the general flame characteristics of an inner flame 18a defining the reducing region where the majority of the oxidizing gas supplied with the reagent burns and an outer flame 18b defining the oxidizing region
35 where the excess fuel oxidizes with any oxidizing gas in the atmosphere.

Fig. 1c shows a schematic of a CCVD apparatus using a Smithell separator 30. The substrate 22 can be placed within the reducing region 32 of the Smithell separator 30 between the inner flame 18a and the outer flame 18b. Alternatively, the substrate 22a can be placed at the exit of the Smithell separator 30, yet still within the reducing region 32, such that substrates 22a larger than the cross-section of the Smithell separator 30 may be coated by moving either the substrate or the apparatus. Additional or other reagents can be supplied to the reducing region 32 of the Smithell separator via supply means 28. The apparatus shown in Fig. 1c has a controlled atmosphere in which, by controlling the fuel gas to oxidizing gas ratio, a reducing region (atmosphere) 32 can be created beyond the inner flame 18a. This apparatus allows for the deposition of materials which require a reducing environment to form quality coatings, such as carbides, nitrides and borides. Sparkers 34 help maintain the flame. A fuel 36, such as hydrogen gas H_2 , NH_3 or other gas is added to the solvent-reagent solution 12 before ignition.

The substrate 22 to be coated is located proximal to flame 18, typically at or near the end 24 of flame 18, but always within the hot gases 20 region. It is preferable that the surface 26 of the substrate 22 which is to be coated is placed facing the flame 18 in some manner, either tangentially as shown in Fig. 1a or obliquely as shown in Fig. 1b, or at any angle to the flame 18 such that the hot gases 20 containing the reagent vapor will contact the surface 26 to be coated. However, as shown in Example 4 and Fig. 8, CCVD can occur on the side of the substrate away from the flame, evidencing that CCVD is not limited to line of sight deposition.

In operation, the chemically reactive compound, or reagent, is mixed with a flammable liquid carrier. It is preferable that the reagent be an organic or inorganic compound which will react in the flame's environment and the carrier be a solvent which is an organic compound, although any reagents which can form a coating and any carriers may be used. It also is preferable that the reagent be dissolved in the carrier as a liquid solvent-reagent solution will spray better in the torch 14, and, consequently, flame better, also resulting in a more homogeneous reagent vapor and subsequent coating on the substrate 22. Throughout this specification, the reagent-carrier mixture, in whatever form, is referred to generally as the solvent-reagent solution 12.

The solvent-reagent solution 12 is supplied to the torch 14. The term torch is used in a general sense to describe any apparatus which can produce a flame from a fuel feed. An oxidant 16 also is supplied to the torch 14 in some fashion. As discussed above, the oxidant 16 may be supplied to the torch 14 as a separate feed,

may be present in the process atmosphere, may be supplied to the process atmosphere or flame ignition point as a separate feed, or may be present in the reagent. The solvent-reagent solution 12 is ignited in the presence of the oxidant 16, creating the flame 18. The oxidant 16 and the solvent combust in the flame 18. The heat
5 generated by the combustion serves two purposes. First, the heat causes liquid reagent solutions to vaporize. Second, the heat heats the substrate 22 to a temperature at which the reagent will coat suitably the substrate 22 so as to result in a uniform, preferred orientation coating, if desired.

After the liquid reagent is vaporized by the heat of combustion of the oxidant
10 16 and the solvent, the reagent vapors leave the flame 18 along with other hot gases 20. The substrate 22 to be coated is placed in a position where the reagent vapors will contact the surface 26 of the substrate 22 to be coated. As the reagent vapors contact the surface 26 to be coated, the reagent vapors condense and form a coating. As discussed in more detail below, the coating may have a preferred orientation, showing
15 heterogeneity.

As discussed above, the solvent-reagent solution 12 in the preferred embodiment is a liquid reagent dissolved in a liquid solvent. However, solid, liquid, vaporous and gaseous reagents can be used, with a liquid or gaseous solvent, as long as the feed to the flame 18 is essentially liquid or gaseous in nature. Although liquid
20 solutions are preferred, the solvent-reagent solution 12 also may contain particles of reagent, typically less than 50%, and preferably less than 10%, of the total solvent-reagent solution 12 volume. Likewise, if particles of reagent are present in the solvent-reagent solution 12, particles of reagent may be present in the hot gases 20. Similarly, particles of reagent may be present in the hot gases 20 in any event,
25 whether or not a complete liquid solvent-reagent solution 12 is used, or one containing particles. The presence of reagent particles generally will not compromise the coating, and coatings with up to 50% particulate matter can be created using the instant method and apparatus.

The following conditions are preferred as the optimum conditions. First, the
30 substrate preferably is located in a zone such that it is heated sufficiently by the flame, or heat of combustion of the solvent-reagent solution 12 and oxidant 16, to allow surface diffusion of the coating along the substrate 22. This temperature is present in the flame 18 to some distance beyond the flame's end 24. Secondly, the metal complexes of the reagent preferably is chemically changed to the final state. For
35 oxides this would occur in a zone between the middle of the flame 18 and the flame's end 24. Finally, the material to be deposited must be in the vapor phase, and can not

be allowed to grow too large (become stable particles). This can be controlled by maintaining a low concentration of solutes, and by minimizing the distance between the surface 26 to be coated and where the oxidation occurs. Combining these different factors predicts the best depositional zone to be in the proximity of the flame's end 24.

5 A plasma torch also can be used in a manner similar to a flame to achieve the same CCVD results. Reagents are sprayed through a plasma torch and deposited onto the substrate. The reagents and other matter fed through the plasma torch are heated and, in turn, heat the substrate surface, much like the flame and hot gases heat the substrate surface in the flame embodiment. Both reacting and/or inert gases can be
10 fed into the plasma torch, resulting in suitable conditions for both CVD and CCVD. In plasma torch CCVD, a lower plasma temperature can be used, compared to conventional plasma spraying, as only enough heat is required to chemically react the reagents; the reactions occur at much lower temperatures than that needed to melt the resulting materials as is required with conventional plasma spraying. Such lower
15 temperatures allow the use of less expensive, safer, and more mobile equipment, and the resulting film quality is comparable to other CVD methods.

CCVD is a more versatile coating technique than existing CVD for some applications. The coating of complex shaped and large parts in the field can be accomplished more simply and economically than conventional CVD processes which
20 must be carried out in a reaction chamber or furnace. Interior surfaces of certain parts also are amenable to coating with CCVD.

Example 1

A coating of the high temperature superconductor $\text{YBa}_2\text{Cu}_3\text{O}_x$. Metal organic reagents containing the Y-Ba-Cu-O precursors were dissolved in xylene. The
25 resulting solution was sprayed from an air brush using 10 percent oxygen enriched air as the propellant gas and oxidant. A single crystal MgO substrate held by metal wires was placed near the flame's end about a foot from the tip of the air brush. Combustion was maintained using a propane soldering torch at the lowest setting with its flame directed at a 45 degree angle to the direction of spray of the sprayed solution as a pilot
30 flame. The deposition was performed in the open atmosphere with no particular set conditions where the specimen cooled rapidly after being coated.

Fig. 2 is an X-ray diffraction (XRD) pattern obtained from this specimen without any post-processing. This pattern indicates that the film is C-axis oriented, which is evidence that CVD occurred by heterogeneous nucleation. A
35 homogeneously nucleated film would produce an XRD pattern similar to that of a randomly oriented powder of YBCO.

Following the collection of the data presented in Fig. 2, the coating was subjected to the following heat treatment in a quartz tube furnace at atmospheric pressure:

1. Heat to about 830°C in a 20/80 (O₂/N₂) atmosphere;
- 5 2. Soak at about 830°C for about 1 h in 20/80 (O₂/N₂) atmosphere;
3. Slow cool to room temperature in 50/50 (O₂/N₂) atmosphere.

Fig. 3 presents the results of a four point resistance vs. temperature determination on the heat treated coating. A superconducting transition is evident beginning between 80 and 85 K.

10

Example 2

A CCVD system was constructed in a fume hood to provide more stable and controllable ambient conditions. Y₂O₃ stabilized ZrO₂ (YSZ) as the coating material was tested on MgO, Al₂O₃ and stainless steel substrates. Two different solvents, ethanol and toluene, and two different metal-organic precursors, 2-ethyl hexanoates
15 (2EH) and acetalacetates (AcAc), were used.

Fig. 6 is an X-ray diffraction pattern of the first run with 10% atomic Y and 90% Zr AcAc in ethanol deposited on a single crystal (100) MgO substrate. The film created is very thin and not complete because of the low solubility of AcAc and the short deposition time (10 min.). Note the high degree of preferred orientation as
20 compared to the standard file card pattern shown in the lower part of the Fig. Preferred orientation is an indication of vapor deposition. Fig. 7 is an X-ray diffraction pattern of the second run using the same atomic ratio but with 2EH precursors in toluene deposited on a similar MgO substrate. Again, note the high degree of preferred orientation (heterogeneous nucleation) as compared to the
25 standard file card pattern shown in the lower part of the Fig. In both cases the substrates were located in the flame near its end at temperatures of about 1200-1300°C. The films of runs 1 and 2 exhibited high degrees of preferred orientation. The film of run 2 was produced with 10 mole percent Y-2EH and 90 mole percent Zr-2EH in toluene deposited on MgO. A cubic YSZ film resulted as would be expected
30 for this composition.

The YSZ coating was deposited on polycrystalline stainless steel from the 2EH-toluene solution using the same procedure. The 2EH concentrations were higher than the AcAc concentrations, so these films are thicker with better coverage. The solubility of the 2EH is much higher than the concentrations used.

Example 3

Fig. 4 is a cross section of a YSZ film on sapphire showing its dense structure and resistance to fracture. The post-deposition substrate fracture shown in Fig. 4 appears not to penetrate into the YSZ, showing the fracture toughness of the coating.

- 5 The substrates were positioned about the flame's end to produce substrate temperatures of approximately 1200°C.

Example 4

- Coatings of BaTiO_3 , Y_2BaCuO_5 , YIG ($\text{Y}_3\text{Fe}_5\text{O}_{12}$ or Yttrium Iron Garnet), Ag and Pt also have been deposited. Fig. 10 shows a cross section of a coating of dense BaTiO_3 on the flame side of an MgO substrate. The BaTiO_3 was deposited using 2EH precursors dissolved in toluene and was deposited on both sides of the substrate, towards and away from the flame. This shows that CCVD is not limited to line of sight deposition, as evidenced by the X-ray diffraction pattern of Fig. 8. Fig. 8 also shows a high degree of preferred orientation as compared to the standard file card pattern shown in the lower part of the Fig. YIG was deposited both with AcAc precursors in ethanol and with 2EH precursors in toluene. Energy dispersive X-ray showed the films were within 10 atomic percent of stoichiometry. XRD indicated that YIG was the major phase in both films. A predominantly Y_2BaCuO_5 film also was deposited and optical observation, the photomicrograph of Fig. 5, suggests epitaxial growth on a (100) MgO substrate. Ag was deposited from a solution of Ag nitrate in ethanol with 10% water. The XRD of Fig. 9, deposited at about 700°C on (100) MgO, showed the Ag (200) peak about 500 times more intense than the maximum peak from a randomly oriented sample. The XRD of the Pt, which was deposited using Pt AcAc in ethanol and toluene, shows variation of the preferred orientation between (100) MgO and α -axis sapphire substrates. Ag, Pt, and all of the above oxides were successfully deposited in the first attempt which shows the great ease and flexibility of this deposition technique.

- CCVD is a more versatile and less expensive coating technique than existing CVD for some applications. In principle, CCVD can be used to deposit coatings of oxides, nitrides, carbides, fluorides, borides, and some elements. The deposition of non-oxide coatings can be achieved, typically by using an open-ended flame enclosure tube with a fuel rich, oxygen poor, mixture and a source of anionic constituents, such as N_2 gas or nitrates for the deposition of nitrides. Non-oxide stable phases may require the use of non-carbon containing fuels so that carbon black would not form. Most depositions occur at atmospheric pressure, but many flames are stable to pressures as low as 10 torr. Alternating compositional layers could be deposited

simply by switching solution or gas sources. The coating of complex shapes, large parts in the field, and the interior surfaces of certain parts with CVD quality is possible using CCVD.

5 The above detailed description of the preferred embodiments and Examples are presented for illustrative purposes only and are not intended to limit the spirit and scope of the present invention, and its equivalents, as defined in the appended claims.

What is claimed is:

1. A method for applying coatings to substrates using chemical vapor deposition comprising the steps of:
 - (a) providing a substrate having at least one surface to be coated;
 - 5 (b) selecting a reagent and a carrier solution and mixing together said reagent and said carrier solution to form a reagent mixture;
 - (c) providing a combustion means;
 - (d) introducing said reagent mixture into said combustion means and combusting said reagent mixture thereby producing a flame and vaporizing at least a
10 portion of said reagent into a vapor phase; and
 - (e) contacting said vapor phase of said reagent with said substrate resulting in the deposition from said vapor phase of a coating onto said substrate.
2. The method as claimed in Claim 1, wherein an oxidant is supplied to said combustion means to assist in combusting said reagent mixture.
- 15 3. The method as claimed in Claim 2, wherein said coating is a crystalline inorganic film.
4. The method as claimed in Claim 2, wherein said reagent mixture is a liquid solution and said coating is a non-crystalline inorganic film.
5. The method as claimed in Claim 2, wherein said reagent mixture is
20 flammable.
6. The method as claimed in Claim 3, wherein a fuel capable of combustion is supplied to said combustion means to fuel said combusting of said reagent mixture.
7. The method as claimed in Claim 4, wherein a fuel capable of
25 combustion is supplied to said combustion means to fuel said combusting of said reagent mixture.
8. The method as claimed in Claim 3, wherein said carrier solution is an organic solvent.
9. The method as claimed in Claim 4, wherein said carrier solution is an
30 organic solvent.
10. The method as claimed in Claim 3, wherein said reagent is gaseous, vaporous or liquid and said carrier solution is gaseous, vaporous or liquid.
11. The method as claimed in Claim 4, wherein said reagent is gaseous, vaporous or liquid and said carrier solution is gaseous, vaporous or liquid.
- 35 12. The method as claimed in Claim 10, wherein said reagent mixture is a liquid solution and said vapor phase consists essentially of vapors of said reagent.

13. The method as claimed in Claim 12, wherein said coating comprises a combination of vapor deposited and spray pyrolysis deposited film of said reagent.

14. The method as claimed in Claim 13, wherein said coating is comprised essentially of spray pyrolysis deposited film of said reagent.

5 15. The method as claimed in Claim 8, wherein said reagent mixture is a liquid solution which comprises solid particles of said reagent and said vapor comprises vapors of said reagent and solid particles of said reagent.

16. The method as claimed in Claim 12, wherein said coating is an essentially heterogeneously nucleated film comprising said reagent.

10 17. The method as claimed in Claim 15, wherein said coating is a film comprising solid particles of said reagent and said reagent.

18. The method as claimed in Claim 17, wherein said coating comprise less than about 50% by volume of said solid particles.

15 19. The method as claimed in Claim 8, wherein said coating is less than about 1000 microns in thickness.

20. The method as claimed in Claim 19, wherein said coating is less than about 100 microns thickness.

20 21. The method as claimed in Claim 1, wherein said substrate is heated predominantly by the heat of combustion produced by combusting said reagent mixture.

22. The method as claimed in Claim 1, wherein said substrate is heated predominantly by a secondary heat source.

23. The method as claimed in Claim 8, wherein said coating is stable in an oxidizing high temperature environment.

25 24. The method as claimed in Claim 8, wherein said coating is not stable in an oxidizing high temperature environment.

25. The method as claimed in Claim 23, wherein said reagent is selected from the group consisting of metalorganic compounds.

30 26. The method as claimed in Claim 24, wherein additional reactants are supplied to said combustion means proximate to but just beyond said flame.

27. The method as claimed in Claim 8, wherein said reagent mixture further comprises non-reactive particles which deposit on said substrate with said coating.

35 28. The method as claimed in Claim 27, wherein said non-reactive particles are molten when striking said substrate.

29. The method as claimed in Claim 1, wherein said flame has a temperature of between about 300°C and 2800°C, said substrate has a surface temperature of between about 100°C and 2200°C, and said deposition occurs at a pressure of between about 10 torr and 10,000 torr.

5 30. The method as claimed in Claim 29, wherein said coating is deposited on said substrate at a deposition rate of between about 0.1µm/hr and 1000µm/hr.

31. The method as claimed in Claim 30, wherein said substrate has a surface temperature of between about 400°C and 1300°C.

10 32. The method as claimed in Claim 4, wherein said coating is less than about 1 mm in thickness.

33. The method as claimed in Claim 32, wherein said flame has a temperature of between about 300°C and 2800°C, said substrate has a surface temperature of between about 100°C and 1500°C, and said deposition occurs at a pressure of between about 10 torr and 10,000 torr.

15 34. The method as claimed in Claim 33, wherein said coating is deposited on said substrate at a deposition rate of between about 0.1µm/hr and 1000µm/hr.

35. The method as claimed in Claim 34, wherein said substrate has a surface temperature of between about 400°C and 1300°C.

20 36. A method for applying coatings to substrates using chemical vapor deposition comprising the steps of:

- (a) providing a substrate having at least one surface to be coated;
- (b) selecting a reagent and a carrier solution and mixing together said reagent and said carrier solution to form a reagent mixture;
- 25 (c) providing a plasma production means;
- (d) introducing said reagent mixture into said plasma production means thereby vaporizing at least a portion of said reagent into a plasma vapor phase; and
- (e) contacting said plasma vapor phase of said reagent with said substrate resulting in the deposition from said plasma vapor phase of a coating onto said
- 30 substrate.

37. The method as claimed in Claim 36, wherein said reagent is gaseous, vaporous or liquid and said carrier solution is gaseous, vaporous or liquid.

38. The method as claimed in Claim 37, wherein said reagent mixture is a liquid solution and said plasma vapor phase consists essentially of vapors of said reagent.

35

39. The method as claimed in Claim 38, wherein said plasma vapor phase has a temperature of between about 800°C and 3500°C.

40. An apparatus for applying coatings to substrates using combustion chemical vapor deposition in ambient conditions using a flame comprising:

- 5 (a) combustion means;
- (b) supply means for supplying a reagent mixture to said combustion means;
- (c) ignition means for igniting said reagent mixture;
- (d) support means for supporting a substrate proximate to said combustion
- 10 means whereby said substrate is supported within a zone through which combustion products resulting from said igniting said reagent mixture pass.

41. The apparatus as claimed in Claim 40, further comprising means for supplying an oxidant to said combustion means.

42. An apparatus for applying inorganic oxide coating to substrates for use
- 15 in combination with combustion chemical vapor deposition in ambient conditions using a flame, comprising a containment means for containing a flammable reagent mixture, an outlet means for releasing said reagent mixture from said containment means, a propellant means for propelling said reagent mixture from said containment means through said outlet means, and an ignition means for igniting said reagent
- 20 mixture.

43. The apparatus as claimed in Claim 42, said apparatus being of a size and configuration so as to be held by and usable by one person's hand.

AMENDED CLAIMS

[received by the International Bureau on 02 August 1994 (02.08.94);
original claims 1-43 replaced by amended claims 1-42 (4 pages)]

What is claimed is:

1. A method for applying inorganic coatings having a minimal amount or no elemental carbon to substrates using chemical vapor deposition comprising the steps of:
 - 5 (a) providing a substrate having at least one surface to be coated;
 - (b) selecting a reagent and a carrier medium and mixing together said reagent and said carrier medium to form a reagent mixture;
 - (c) providing a combustion means;
 - (d) providing an oxidant to said combustion means to assist in combusting
10 said reagent mixture and to minimize elemental carbon deposition in said resulting coating;
 - (e) introducing said reagent mixture into said combustion means and combusting said reagent mixture thereby producing a flame and vaporizing at least a portion of said reagent into a vapor phase; and
15 (f) contacting said vapor phase of said reagent with said substrate resulting in the deposition from said vapor phase of an inorganic coating onto said substrate.
2. The method as claimed in Claim 1, wherein said coating is a crystalline inorganic film.
3. The method as claimed in Claim 1, wherein said reagent mixture is a
20 liquid solution and said coating is a non-crystalline inorganic film.
4. The method as claimed in Claim 1, wherein said reagent mixture is flammable.
5. The method as claimed in Claim 3, wherein a fuel capable of combustion is supplied to said combustion means to fuel said combusting of said
25 reagent mixture.
6. The method as claimed in Claim 4, wherein a fuel capable of combustion is supplied to said combustion means to fuel said combusting of said reagent mixture.
7. The method as claimed in Claim 3, wherein said carrier medium is a
30 liquid organic solvent.
8. The method as claimed in Claim 4, wherein said carrier medium is a liquid organic solvent.
9. The method as claimed in Claim 3, wherein said reagent is in a non-solid state and said carrier medium is in a non-solid state.
- 35 10. The method as claimed in Claim 4, wherein said reagent is in a non-solid state and said carrier medium is in a non-solid state.

11. The method as claimed in Claim 10, wherein said reagent mixture is a liquid solution and said vapor phase consists essentially of vapors of said reagent.
12. The method as claimed in Claim 12, wherein said coating comprises a combination of vapor deposited and spray pyrolysis deposited film of said reagent.
- 5 13. The method as claimed in Claim 13, wherein said coating is comprised essentially of spray pyrolysis deposited film of said reagent.
14. The method as claimed in Claim 8, wherein said reagent mixture is a liquid solution which comprises solid particles of said reagent and said vapor comprises vapors of said reagent and solid particles of said reagent.
- 10 15. The method as claimed in Claim 12, wherein said coating is an essentially heterogeneously nucleated film comprising said reagent.
16. The method as claimed in Claim 15, wherein said coating is a film comprising solid particles of said reagent and said reagent.
17. The method as claimed in Claim 17, wherein said coating comprises less
15 than about 50% by volume of said solid particles.
18. The method as claimed in Claim 8, wherein said coating is less than about 1000 microns in thickness.
19. The method as claimed in Claim 19, wherein said coating is less than about 100 microns in thickness.
- 20 20. The method as claimed in Claim 1, wherein said substrate is heated predominantly by the heat of combustion produced by combusting said reagent mixture.
21. The method as claimed in Claim 1, wherein said substrate is heated predominantly by a secondary heat source.
- 25 22. The method as claimed in Claim 8, wherein said coating is thermodynamically stable in an oxidizing environment having a temperature of approximately 300°C or higher.
23. The method as claimed in Claim 8, wherein said coating is not thermodynamically stable in an oxidizing environment having a temperature of
30 approximately 300°C or higher.
24. The method as claimed in Claim 23, wherein said reagent is a metalorganic compound.
25. The method as claimed in Claim 24, wherein additional reactants are supplied to said combustion means proximate to but just beyond said flame.
- 35 26. The method as claimed in Claim 8, wherein said reagent mixture further comprises non-reactive particles which deposit on said substrate with said coating.

27. The method as claimed in Claim 27, wherein said non-reactive particles are molten when striking said substrate.

28. The method as claimed in Claim 1, wherein said flame has a temperature of between about 300°C and 2800°C, said substrate has a surface temperature of between about 100°C and 2200°C, and said deposition occurs at a pressure of between about 10 torr and 10,000 torr.

29. The method as claimed in Claim 29, wherein said coating is deposited on said substrate at a deposition rate of between about 0.1µm/hr and 1000µm/hr.

30. The method as claimed in Claim 30, wherein said substrate has a surface temperature of between about 400°C and 1300°C.

31. The method as claimed in Claim 4, wherein said coating is less than about 1 mm in thickness.

32. The method as claimed in Claim 32, wherein said flame has a temperature of between about 300°C and 2800°C, said substrate has a surface temperature of between about 100°C and 1500°C, and said deposition occurs at a pressure of between about 10 torr and 10,000 torr.

33. The method as claimed in Claim 33, wherein said coating is deposited on said substrate at a deposition rate of between about 0.1µm/hr and 1000µm/hr.

34. The method as claimed in Claim 34, wherein said substrate has a surface temperature of between about 400°C and 1300°C.

35. A method for applying inorganic coatings having a minimal amount or no elemental carbon to substrates using chemical vapor deposition comprising the steps of:

- (a) providing a substrate having at least one surface to be coated;
- (b) selecting a reagent and a carrier medium and mixing together said reagent and said carrier medium to form a reagent mixture;
- (c) providing a plasma production means capable of being operated so as to minimize the formation of elemental carbon;
- (d) introducing said reagent mixture into said plasma production means thereby vaporizing at least a portion of said reagent into a plasma vapor phase comprising a minimal amount or not elemental carbon; and
- (e) contacting said plasma vapor phase of said reagent with said substrate resulting in the deposition from said plasma vapor phase of an inorganic coating onto said substrate.

36. The method as claimed in Claim 35, wherein said reagent is gaseous, vaporous or liquid and said carrier medium is gaseous, vaporous or liquid.

37. The method as claimed in Claim 36, wherein said reagent mixture is a liquid solution and said plasma vapor phase consists essentially of vapors of said reagent.

38. The method as claimed in Claim 37, wherein said plasma vapor phase has a temperature of between about 800°C and 3500°C.

39. An apparatus for applying coatings to substrates using combustion chemical vapor deposition in ambient conditions using a flame comprising:

- 10 (a) combustion means;
- (b) supply means for supplying a reagent mixture to said combustion means;
- (c) ignition means for igniting said reagent mixture;
- (d) support means for supporting a substrate proximate to said combustion
- 15 means whereby said substrate is supported within a zone through which combustion products resulting from said igniting said reagent mixture pass.

40. The apparatus as claimed in Claim 40, further comprising means for supplying an oxidant to said combustion means.

41. An apparatus for applying inorganic oxide coating to substrates for use in combination with combustion chemical vapor deposition in ambient conditions using a flame, comprising a containment means for containing a flammable reagent mixture, an outlet means for releasing said reagent mixture from said containment means, a propellant means for propelling said reagent mixture from said containment means through said outlet means, and an ignition means for igniting said reagent mixture.

42. The apparatus as claimed in Claim 42, said apparatus being of a size and configuration so as to be held by and usable by one person's hand.

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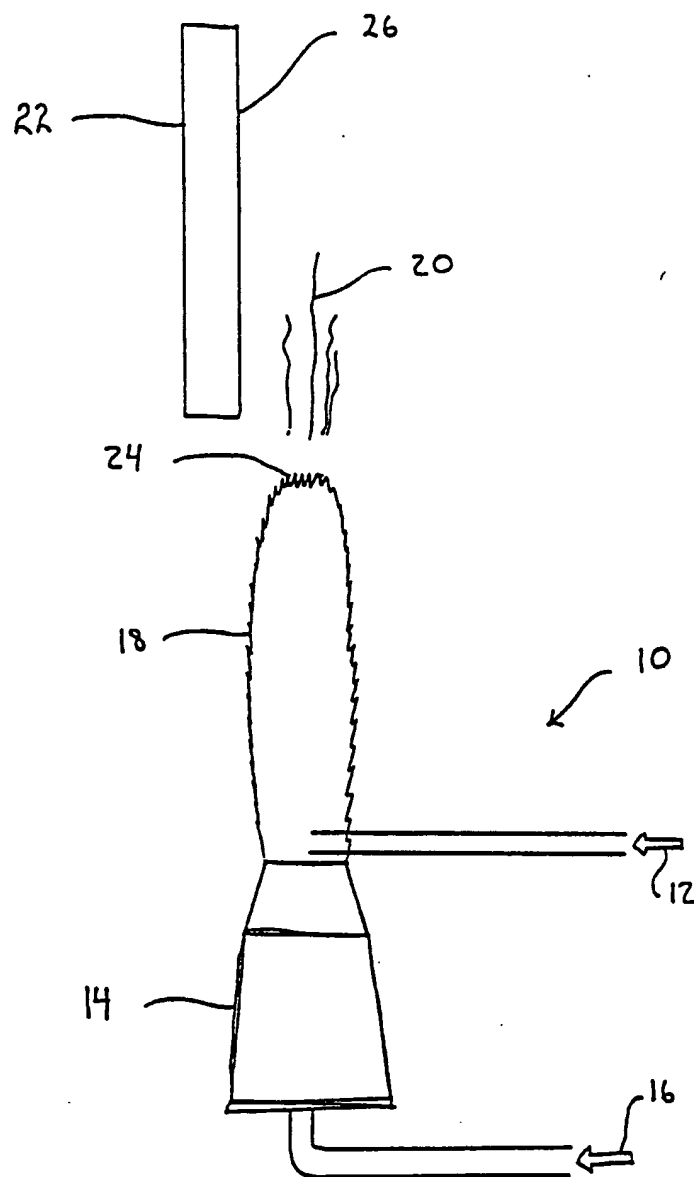


FIG. 1a

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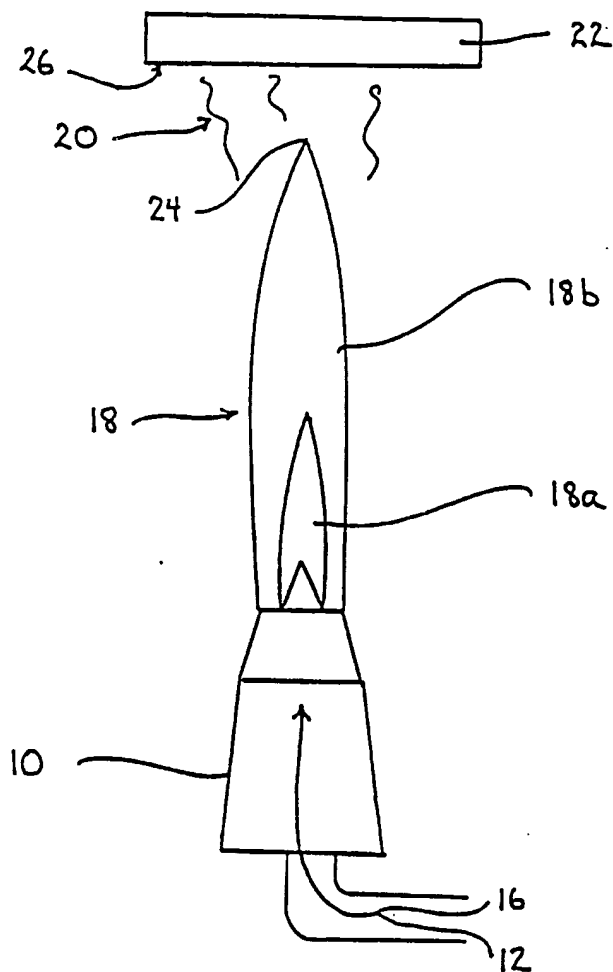


FIG. 1b

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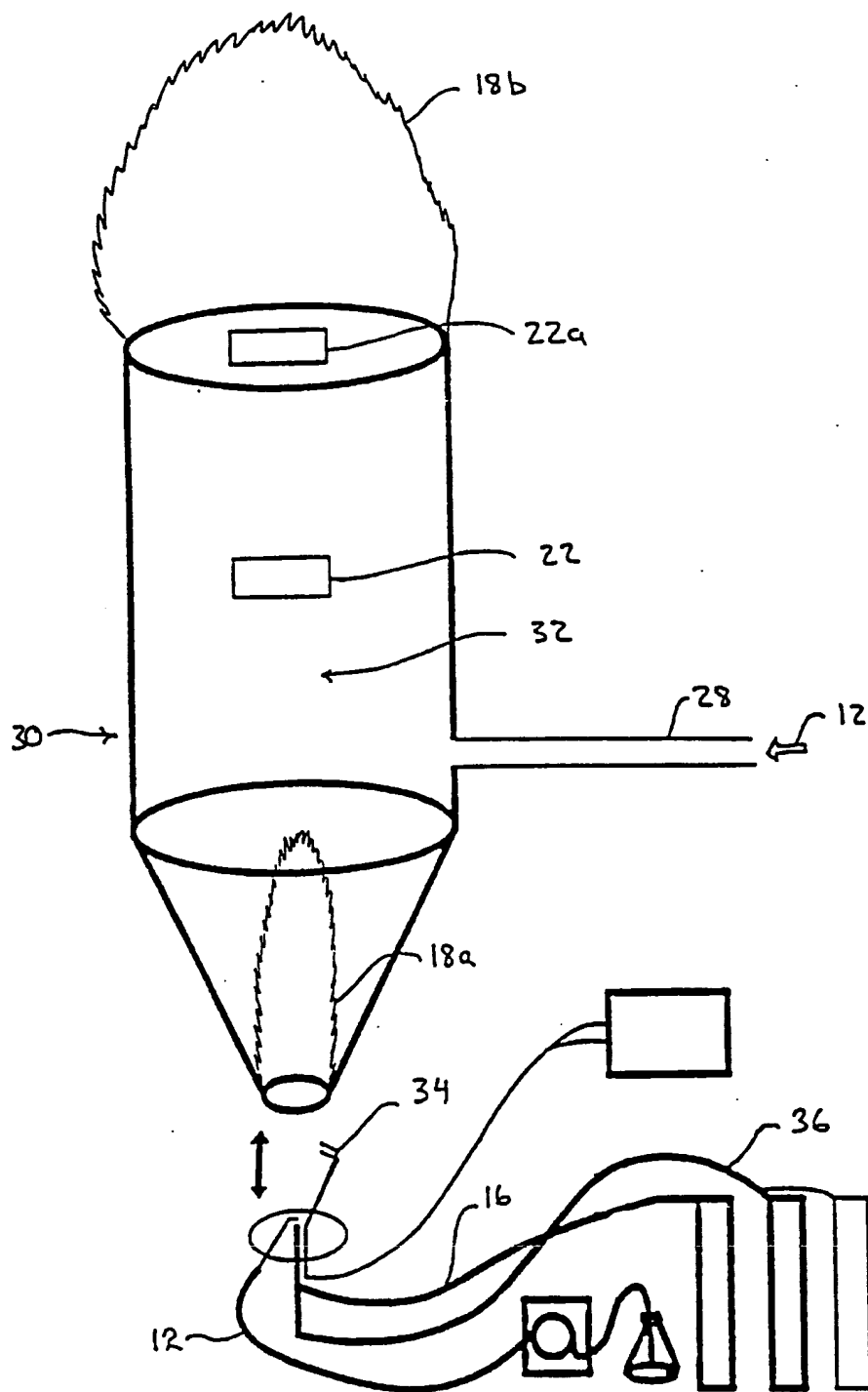


FIG. 1c

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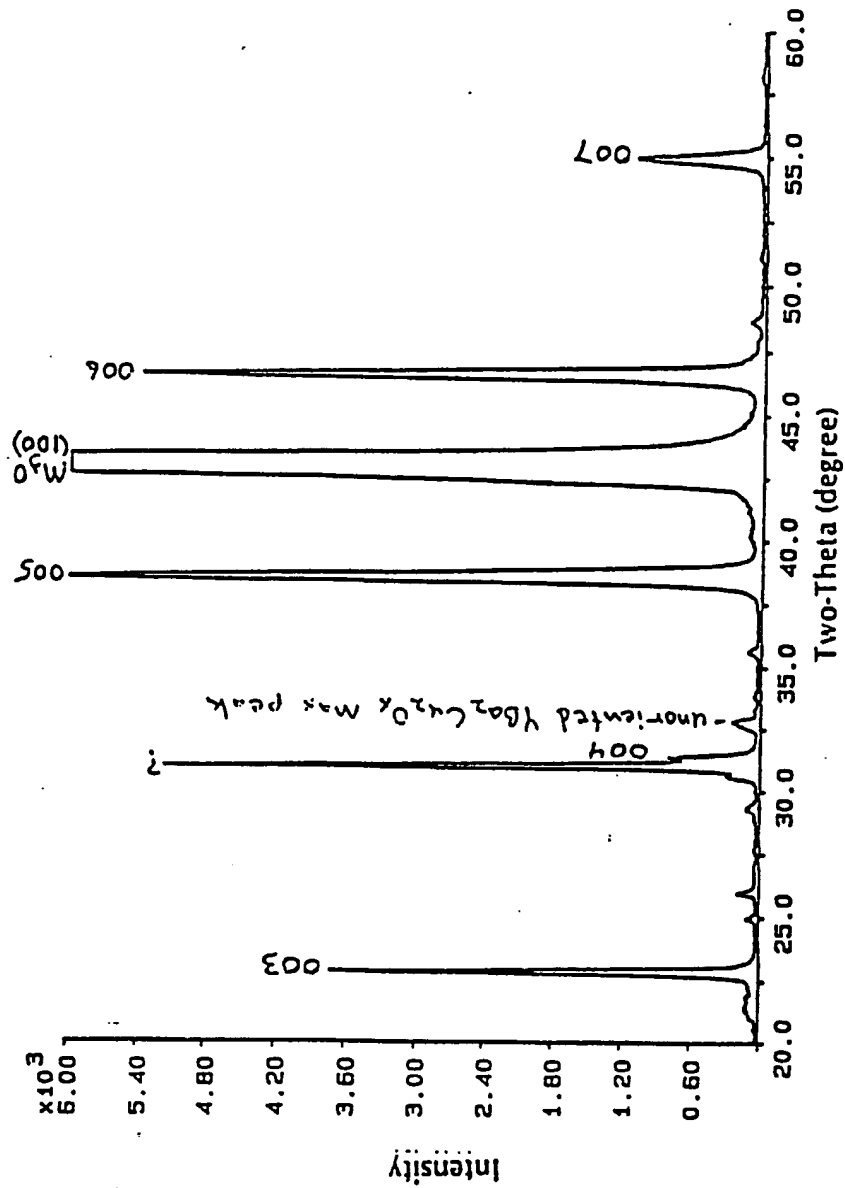


FIG. 2

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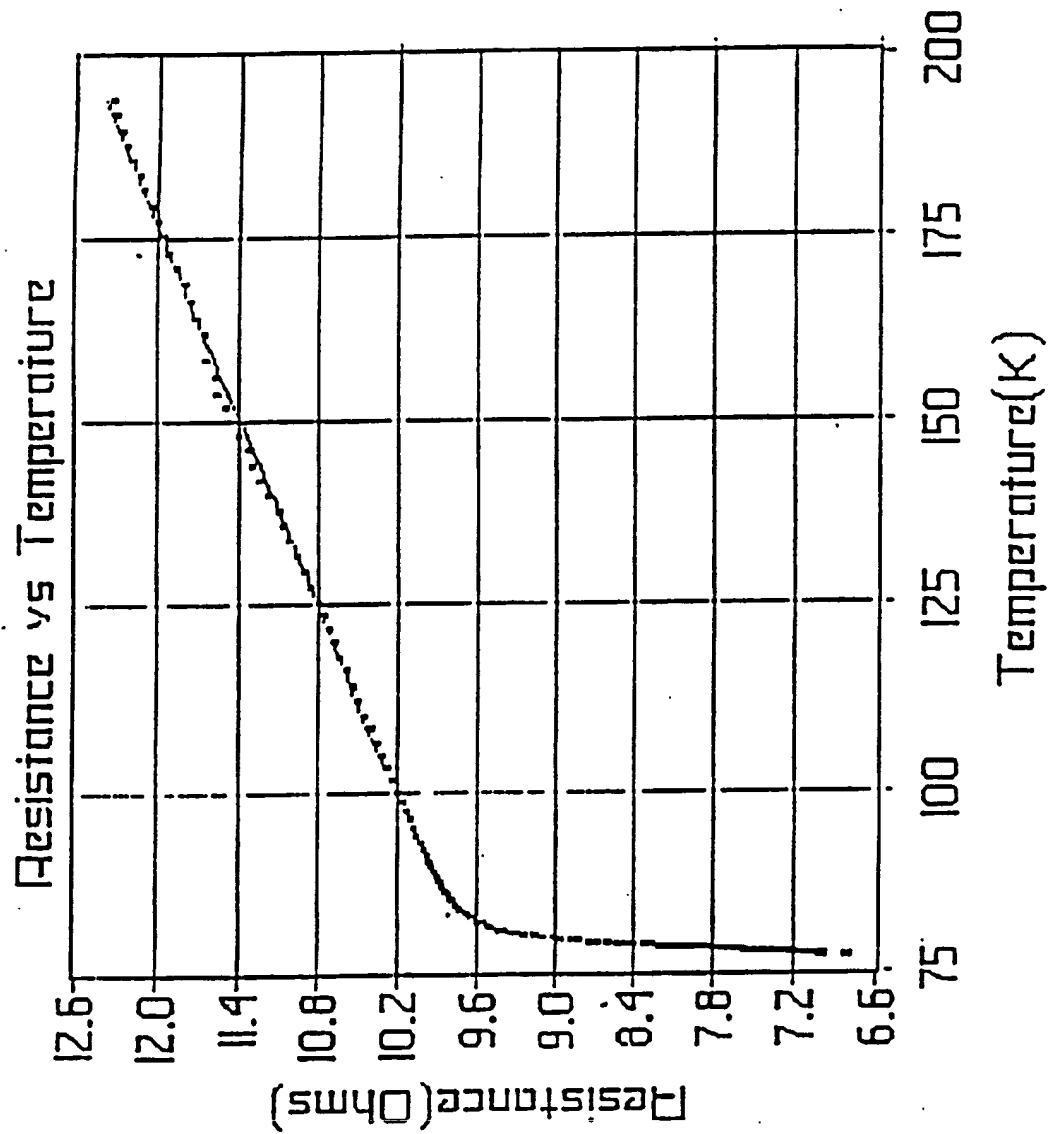


FIG. 3

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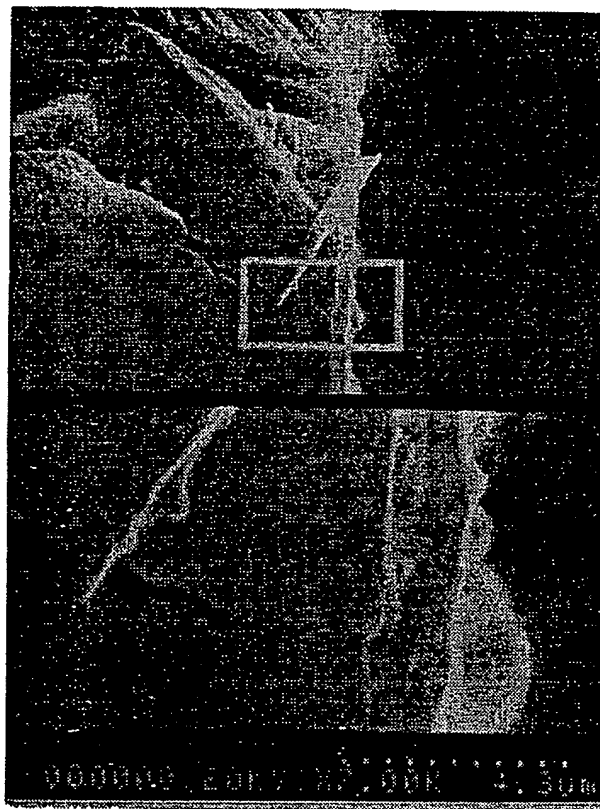


FIG. 4

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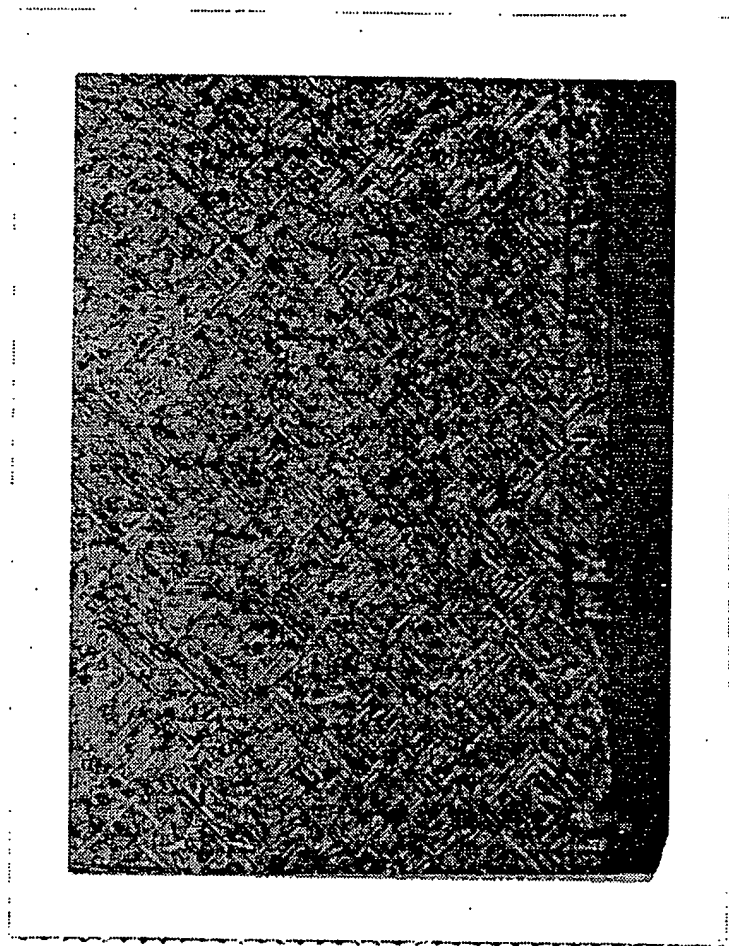


FIG. 5

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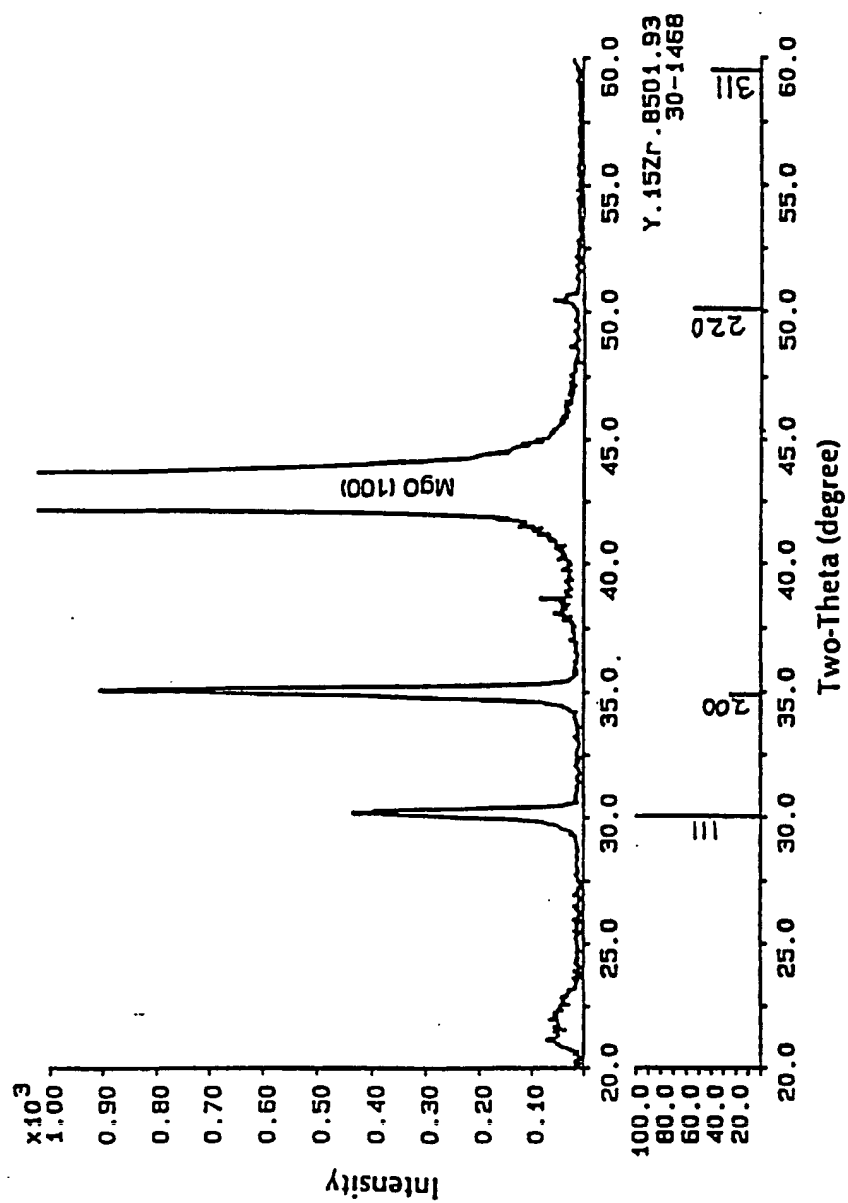


FIG. 6

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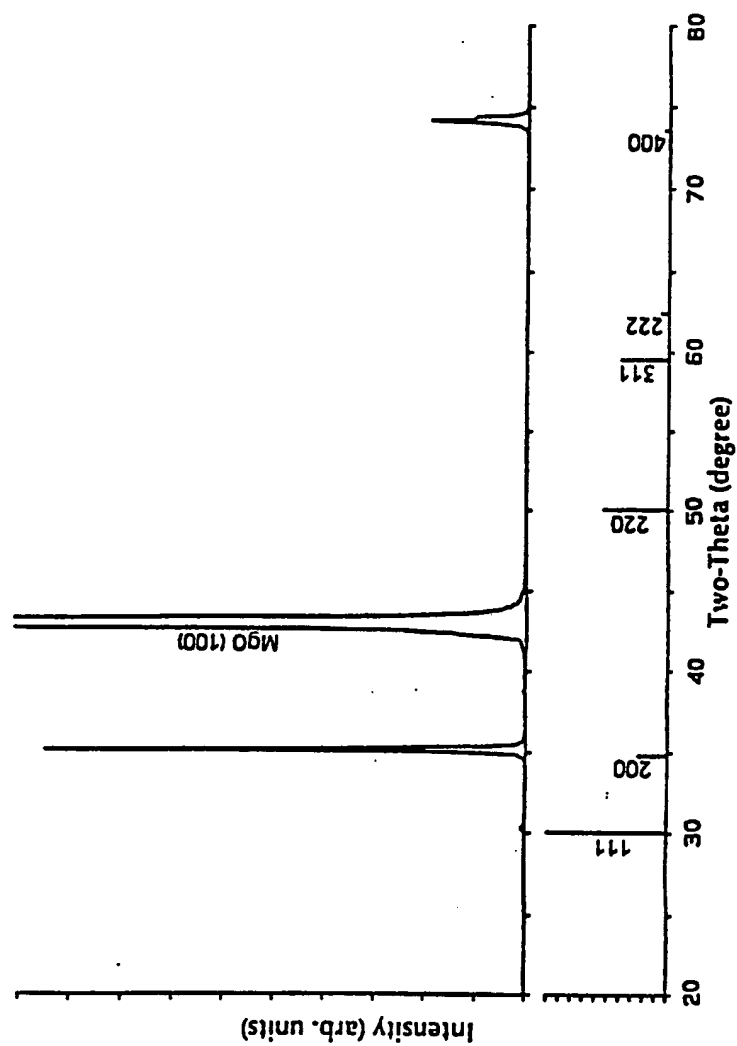


FIG. 7

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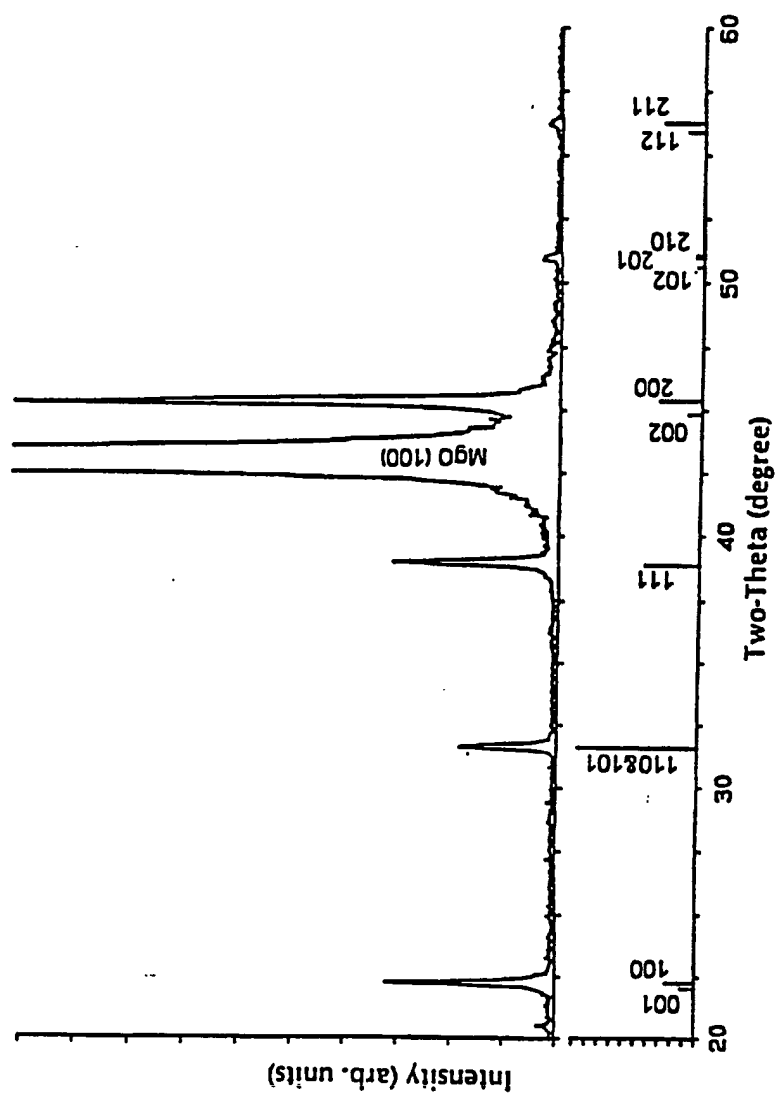


FIG. 8

11/12

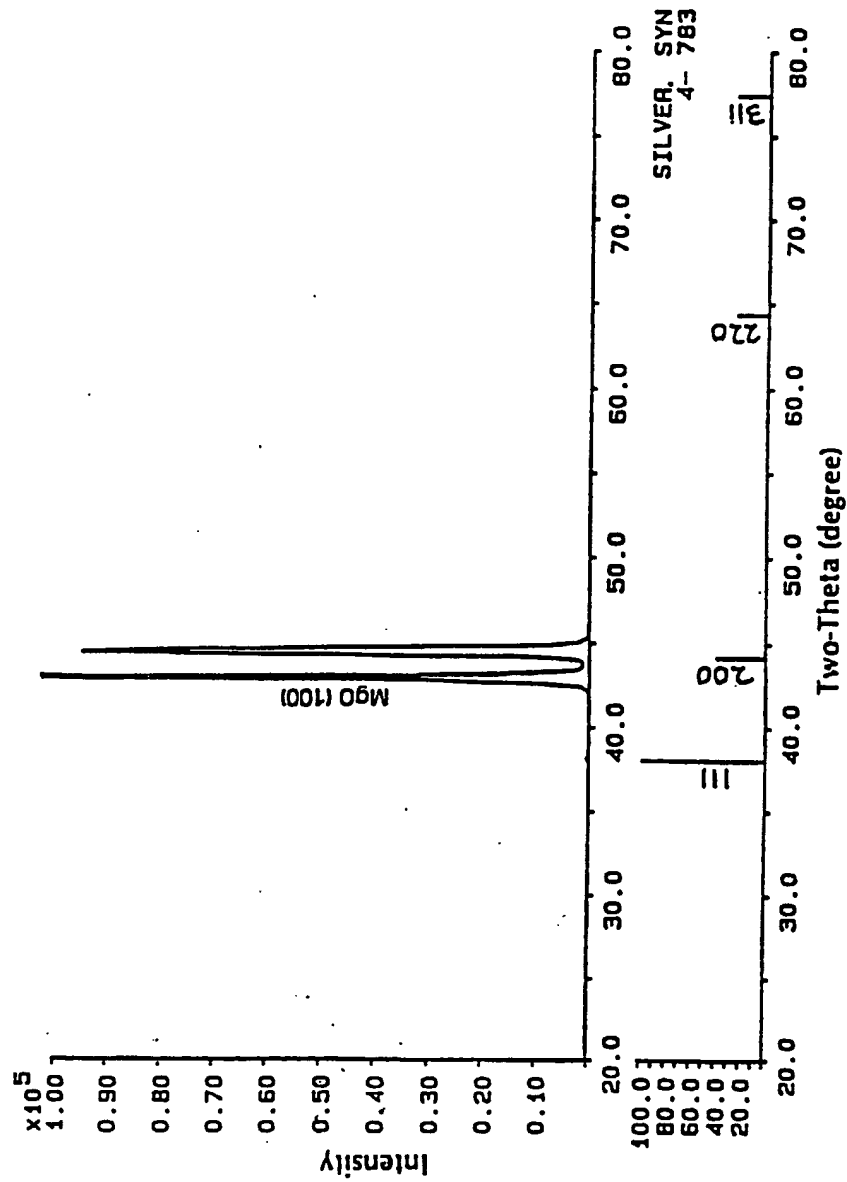


FIG. 9

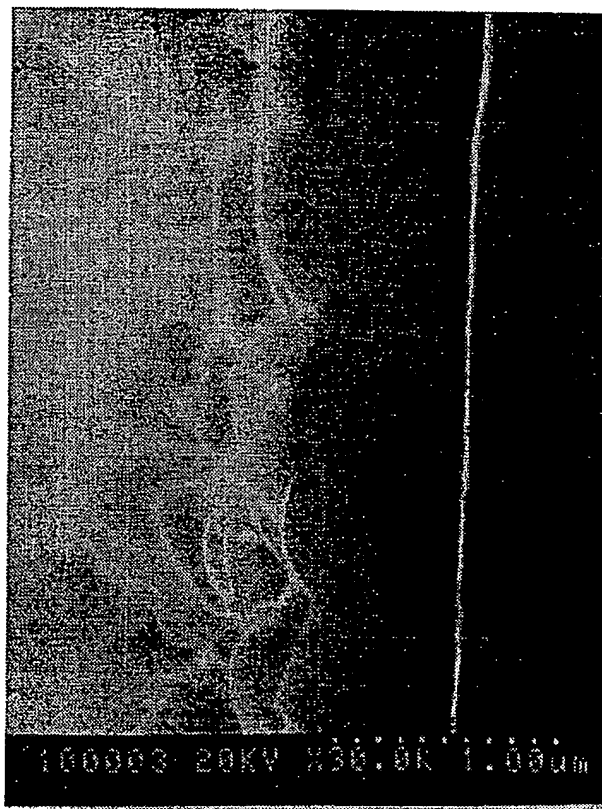


FIG. 10

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INTERNATIONAL SEARCH REPORT

 International application No.
PCT/US94/03193

A. CLASSIFICATION OF SUBJECT MATTER

IPC(5) : C23C 16/00, 16/50

US CL : 427/569,573,248.1,255.1,255.3;118/724,728

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 427/569,573,248.1,255.1,255.3;118/724,728

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P,Y	US,A, 5,215,788 (MURAYAM ET AL.) 01 JUNE 1993, SEE COL. 1 LINES 30-46, COL. 2 LINE 65- COL. 3 LINE 6	ALL
Y	US,A, 5,174,983 (SNAIL) 29 DECEMBER 1992, SEE COL. 1 LINES 8-10, COL. 3, LINES 25-36, COL. 2 LINE 63-COL. 3 LINE 18	ALL
Y	US,A, 4,957,591 (SATO ET AL) 18 SEPTEMBER 1990, SEE COL. 1 LINES 8-10, COL. 2 LINES 60-62	ALL
A	US,A, 4,822,466 (RABALAIS ET AL) 18 APRIL 1989 SEE COL. 2 LINE 45- COL. 3 LINE 29	ALL
A,P	US,A, 5,275,798 (AIDA) 04 JANUARY 1994 SEE ABSTRACT	ALL

☒ Further documents are listed in the continuation of Box C. ☐ See patent family annex.

Special categories of cited documents:		* T later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention	
* A	document defining the general state of the art which is not considered to be of particular relevance		
* E	earlier document published on or after the international filing date	* X	document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
* L	document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	* Y	document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
* O	document referring to an oral disclosure, use, exhibition or other means		
* P	document published prior to the international filing date but later than the priority date claimed	* &	document member of the same patent family

Date of the actual completion of the international search

04 MAY 1994

Date of mailing of the international search report

JUN 02 1994

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Box PCT
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Facsimile No. (703) 305-3230

Authorized officer

SHRIVE BECK

Telephone No. (703) 308-0661

INTERNATIONAL SEARCH REPORT

International application No.
PCT/US94/03193

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US,A, 5,178,905 (KANAI ET AL.) 12 JANUARY 1993, SEE COL. 3 LINES 17-43	ALL